TABLE I

Solubility of Phenanthrene, 25°

The pressure in atmospheres is followed by the solubility in mole percentage in parentheses.

n-Hexane

1 (3.26), 500 (2.72), 1000 (2.26), 2000 (1.80), 4300 (1.04), 7150 (0.50), 8750 (0.36)

n-Heptane

1 (4.01), 500 (3.21), 900 (2.92), 1000 (2.72), 2000 (1.84), 3430 (1.11), 5000 (0.84), 7000 (0.52)

n-Octane

1 (4.64), 490 (3.81), 1000 (2.84), 1960 (1.97), 3850 (1.20), 5200 (0.88)

CS_2

1 (23.5), 500 (16.2), 1000 (12.5), 2000 (7.3), 4000 (4.5), 6000 (2.9), 7000 (2.2)

TABLE II

SOLUBILITY OF SnI4

The pressure is given in atmospheres followed by the solubility in mole percentage in parentheses.

n-Hexane

1 (0.470), 10 (0.443), 480 (0.315), 1000 (0.199), 2000 (0.099), 3100 (0.057), 5100 (0.047), 7200 (0.033), 9100 (0.019)

n-Heptane

1 (0.553), 470 (0.383), 980 (0.163), 2000 (0.048), 3000 (0.031), 4600 (0.019), 7200 (0.018)

n-Octane

1 (0.621), 500 (0.429), 1000 (0.245), 1500 (0.148), 2000 (0.115)

CS_2

1 (14.61), 1000 (7.99), 2000 (5.64), 3600 (3.45), 5000 (1.96), 7000 (0.77), 10,000 (0.11)

TABLE III

SOLUBILITY OF C2Cl6

The pressure in atmospheres is followed by the solubility in mole percentage in parentheses.

n-Hexane

1 (13.92), 400 (9.84), 1000 (6.36), 2000 (3.40), 3300 (1.72), 5000 (0.64), 5830 (0.29), 6750 (0.26)

n-Heptane

1 (15.18), 410 (10.48), 1000 (6.79), 2000 (2.30), 2970 (1.63), 4000 (0.83), 5000 (0.40)

n-Octane

1 (15.72), 400 (10.35), 1000 (6.33), 2000 (3.44)

CS_2

1 (19.5), 500 (12.0), 1000 (8.0), 1970 (4.1), 3400 (2.3), 5000 (1.3), 7000 (0.31)

2-Methylpentane

1 (13.02), 400 (9.15), 1000 (5.76), 1950 (3.14), 3350 (1.43), 5000 (0.52), 6900 (0.22)

3-Methylpentane

1 (13.52), 400 (9.56), 1000 (6.21), 2000 (3.15), 3500 (1.19), 5000 (0.61), 7000 (0.18)

2,3-Dimethylbutane

1 (13.15), 400 (9.19), 990 (5.74), 1970 (2.83), 3500 (1.15), 4950 (0.51), 6800 (0.14)

2,2-Dimethylbutane

1 (12.02), 400 (8.48), 990 (5.41), 2000 (2.72), 3500 (0.98), 4500 (0.45)

TABLE IV

SOLUBILITY OF ANTHRACENE

The pressure in atmospheres is followed by the solubility in mole percentage in parentheses.

CS

1 (0.84), 240 (0.70), 500 (0.59), 1000 (0.41), 2000 (0.27), 4000 (0.13)

various temperatures by Dorfman and Hildebrand.¹ The density coefficient of solubility varies considerably more rapidly at constant pressure than at constant temperature. A similar result was found for SnI₄ in n-heptane.

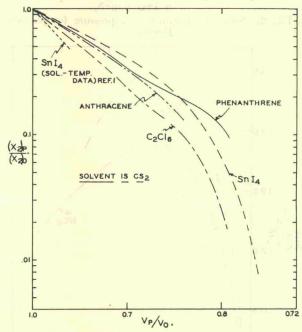


Fig. 1.—Relative solubility vs. relative molar volume of solvent.

It is useful to compare our atmospheric pressure data with values in the literature. In Table V

TABLE V

Comparison of Solubilities Obtained in This Work with Published Solubility Values of SnI₄ (Mole %)

Solvent	Dorfman and Hildebrand ¹	This
Heptane	0.533	0.552
CS_2	14.64	14.61

Solubility of phenanthrene (mole %)

Solvent	Ellefson and Beebe	This work Eastman	V Recrystallized
CS_2	25.5	23.5	21.6
n-Hexane	4.2	3.26	3.09
So	lubility of anthr	racene (mole	%)

Solvent Ref. 2 This work CS_2 1.09 0.84

we see such a comparison. We find excellent agreement for the solubility of SnI₄ in CS₂ and in heptane, but no agreement for the solubility of

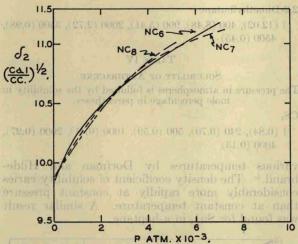


Fig. 2.—Solubility parameter vs. pressure for phenanthrene.

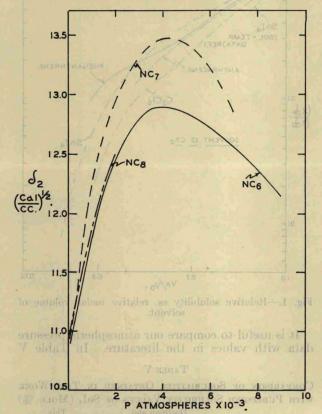


Fig. 3.—Solubility parameters vs. pressure for SnI4.

phenanthrene and anthracene in heptane. We have no good explanation of this. We tried two different batches of Eastman phenanthrene, and recrystallized one batch several times. We never obtained any variation from batch to batch greater than 10%, and the more highly purified batches deviated most widely from Hildebrand's values.

Comparison of Theory and Results.—By far the most widely used theory of solutions is that developed by Scatchard and Hildebrand. Recently theories with a sounder basis in statistical mechanics have been developed by Guggenheim,⁵

(5) E. A. Guggenheim, "Mixtures," Oxford Univ. Press, New York, N. Y., 1952. Kirkwood⁶ and Prigogine and co-workers.⁷ These, however, are not readily applied to a discussion of solubility under pressure.

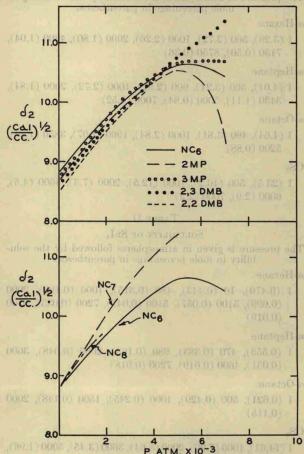


Fig. 4.—Solubility parameter vs. pressure for C2Cl6.

To discuss our results we shall use the S-H theory. This theory gives for the partial molal free energy of the solute

$$\Delta \bar{F}_2 = V_2 \varphi_1^2 (\delta_2 - \delta_1)^2 + RT \ln X_2$$
 (1)

if the entropy of mixing is ideal, or

$$\left[\Delta \bar{F}_{2} = V_{2}\varphi_{1}^{2}(\delta_{2} - \delta_{1})^{2} + RT \ln \varphi_{2} + \varphi_{1}\left(1 - \frac{V_{2}}{V_{1}}\right)\right]$$
 (2)

if the Flory-Huggins entropy is used. Here

 V_i = molal vol. of i (of the supercooled liquid for the solute)

 X_2 = mole fraction of solute (measured)

 φ_i = vol. fraction of i

 δ_i = solubility parameter of i

 $=\left(\frac{-E}{V}\right)^{-1}$

where -E = cohesive energy, at one atmosphere, the energy of vaporization into a perfect gas.

It is not hard to show that

$$\overline{\Delta F_2} = RT \ln X_2^i \tag{3}$$

(8) J. H. Hildebrand and R. L. Scott, "The Solubility on Non-electrolytes," 3rd Ed., Reinhold Publ. Corp., New York, N. Y., 1950.

⁽⁶⁾ Z. Salzberg and J. H. Kirkwood, J. Chem. Phys., 20, 1538 (1952); 21, 2169 (1953).

⁽⁷⁾ I. Prigogine and V. Mathot, *ibid.*, **20**, 49 (1952); I. Prigogine and A. Bellemans, *Disc. Faraday Soc.*, No. 15, 80 (1953); I. Prigogine, N. Trappeniers and V. Mathot, *ibid.*, No. 15, 93 (1953). See also other articles referred to in these papers.